



Acronyms used in the following formulas are defined in the WellSharp Acronyms document, available on the secure Provider Resources webpage. For instructions on rounding numbers when making calculations, refer to the following rounding rules and recommendations. Carry the rounded values forward into subsequent calculations.

**ROUNDING RULES**

- When calculating Kill Mud Weight, **ROUND UP** to one decimal place (for example: round up 10.73 ppg to 10.8 ppg; round up 11.03 ppg to 11.1 ppg).
- When calculating Leak Off Test Equivalent Mud Weight, **ROUND DOWN** to one decimal place (for example: round down 11.76 ppg to 11.7 ppg; round down 13.89 ppg to 13.8 ppg).
- When calculating Pressure Reduction Schedule, **ROUND DOWN** to a whole number (for example: round down 21.6 psi/100 stks to 21 psi/100 stks).
- If the Kill Mud Weight or Leak Off values are to be used in subsequent calculations, use the rounded value in the future calculation. Do not use the unrounded calculated value.

**ROUNDING RECOMMENDATIONS**

See Table to right where:

X= Whole number

X.XXXX = Number with 4 decimal places

MEASUREMENT	UNITS	ROUNDING and ANSWER FORMAT
Depth	feet	X
Pressure	psi	X
Pressure Gradient	psi/foot	X.XXXX
Mud Weight	ppg	X.X
Volume	bbls	X.X
Capacity and Displacement	bbls/foot	X.XXXX
Pump Speed in strokes per minute	SPM	X
Strokes	stk or stks	X
Speed in feet per hour	feet/hour	X
Area	in <sup>2</sup>	X.XXXX
Force	lbs	X
Buoyancy Factor	Unitless	X.XXXX
Wait and Weight Pressure Reduction Schedule	psi/100 stks or psi/10 steps*	X

\* 10 steps = Surface to Bit strokes divided by 10.

1. FORCE (*lbs*) = Pressure<sub>psi</sub> x Diameter<sup>2</sup> x 0.7854 (*Diameter in inches*)
2. AREA (RECTANGULAR) = Length x Width
3. AREA (CIRCULAR) = Diameter<sup>2</sup> x 0.7854
4. PRESSURE (*psi*) = Force<sub>lbs</sub> ÷ Diameter<sup>2</sup> ÷ 0.7854
5. RECTANGULAR TANK VOLUME (*bbls*) = (Length<sub>ft</sub> x Width<sub>ft</sub> x Height<sub>ft</sub>) ÷ 5.615
6. RECTANGULAR TANK CAPACITY (*bbls/ft*) = Length<sub>ft</sub> x Width<sub>ft</sub> x 0.178
7. RECTANGULAR TANK CAPACITY (*bbls/in*) = Length<sub>ft</sub> x Width<sub>ft</sub> x 0.0148
8. VERTICAL CYLINDRICAL TANK VOLUME (*bbls*) = Capacity<sub>bbls/ft</sub> x Height<sub>ft</sub>
9. VERTICAL CYLINDRICAL TANK CAPACITY (*bbls/ft*) = Tank diameter<sub>ft</sub><sup>2</sup> ÷ 7.148
10. TUBULAR CAPACITY (*bbls/ft*) = ID<sup>2</sup> ÷ 1029.4 (*ID = Internal Diameter of Tubular*)
11. ANNULAR CAPACITY (*bbls/ft*) = (D<sup>2</sup> - d<sup>2</sup>) ÷ 1029.4 (*D = Hole Diameter or Casing ID, d = Outside Diameter of Tubular*)
12. HEIGHT OF FLUID IN A PIPE OR ANNULUS (*ft*) = Kick Volume<sub>bbls</sub> ÷ Annular Capacity<sub>bbls/ft</sub> or Pipe Capacity<sub>bbls/ft</sub>
13. HYDROSTATIC PRESSURE (*psi*) = Mud Weight<sub>ppg</sub> x 0.052 x TVD<sub>ft</sub>
14. HYDROSTATIC PRESSURE GRADIENT (*psi/ft*) = Mud Weight<sub>ppg</sub> x 0.052
15. FORMATION PRESSURE (*psi*) = Hydrostatic Pressure in Drill String<sub>psi</sub> + SIDPP<sub>psi</sub>  
(*also referred to as Bottomhole Pressure at Shut In*)
16. MUD WEIGHT (*ppg*) = Pressure Gradient<sub>psi/ft</sub> ÷ 0.052 or Pressure<sub>psi</sub> ÷ TVD<sub>ft</sub> ÷ 0.052
17. EQUIVALENT MUD WEIGHT (*ppg*) = Pressure<sub>psi</sub> ÷ 0.052 ÷ TVD<sub>ft</sub> or (Surface Pressure<sub>psi</sub> ÷ TVD<sub>ft</sub> ÷ 0.052) + Mud Weight<sub>ppg</sub>

18. EQUIVALENT CIRCULATING DENSITY (ppg) =  $[\text{Annular Pressure Loss}_{\text{psi}} \div 0.052 \div \text{TVD}_{\text{ft}}] + \text{Original Mud Weight}_{\text{ppg}}$
19. KILL MUD WEIGHT (ppg) =  $[\text{SIDPP}_{\text{psi}} \div 0.052 \div \text{TVD}_{\text{ft}}] + \text{Original Mud Weight}_{\text{ppg}}$
20. INITIAL CIRCULATING PRESSURE (psi) =  $\text{Slow Circulating Rate Pressure}_{\text{psi}} + \text{SIDPP}_{\text{psi}}$
21. FINAL CIRCULATING PRESSURE (psi) =  $\text{Slow Circulating Rate Pressure}_{\text{psi}} \times [\text{Kill Mud Weight}_{\text{ppg}} \div \text{Original Mud Weight}_{\text{ppg}}]$
22. NEW PUMP PRESSURE WITH NEW SPM (psi) =  $\text{Current Pressure}_{\text{psi}} \times [\text{New SPM} \div \text{Old SPM}]^2$  **(only approximate!)**
23. NEW PUMP PRESSURE WITH NEW MUD WEIGHT (psi) =  $\text{Current Pressure}_{\text{psi}} \times [\text{New Mud Weight} \div \text{Old Mud Weight}]$  **(only approximate!)**
24. MAXIMUM ALLOWABLE MUD WEIGHT (ppg)  
(Fracture Mud Weight) =  $[\text{Surface Leak Off}_{\text{psi}} \div 0.052 \div \text{Shoe TVD}_{\text{ft}}] + \text{Test Mud Weight}_{\text{ppg}}$
25. MAASP or MACP (psi) =  $[\text{Maximum Allowable Mud Weight}_{\text{ppg}} - \text{Current Mud Weight}_{\text{ppg}}] \times 0.052 \times \text{Shoe TVD}_{\text{ft}}$
26. NEW MAASP AFTER KILL (psi) =  $[\text{Maximum Allowable Mud Weight}_{\text{ppg}} - \text{Kill Mud Weight}_{\text{ppg}}] \times 0.052 \times \text{Shoe TVD}_{\text{ft}}$
27. ADDITIONAL MUD RETURNED BY SLUG (bbls) =  $[(\text{Slug Weight}_{\text{ppg}} \div \text{Mud Weight}_{\text{ppg}}) - 1] \times \text{Slug Volume}_{\text{bbls}}$
28. TOTAL MUD RETURNED BY SLUG (bbls) =  $(\text{Slug Weight}_{\text{ppg}} \div \text{Mud Weight}_{\text{ppg}}) \times \text{Slug Volume}_{\text{bbls}}$
29. LEVEL DROP AFTER PUMPING A SLUG (ft) =  $[(\text{Slug Weight}_{\text{ppg}} \div \text{Mud Weight}_{\text{ppg}}) - 1] \times \text{Slug Volume}_{\text{bbls}} \div \text{Drill Pipe Capacity}_{\text{bbls/ft}}$
30. RISER MARGIN (ppg) =  $[(\text{Riser Mud Hydrostatic}_{\text{psi}} - \text{Seawater Hydrostatic}_{\text{psi}}) \div 0.052] \div (\text{Well TVD}_{\text{ft}} - \text{Water Depth}_{\text{ft}} - \text{RKB-MSL}_{\text{ft}})$
31. CASING (or CHOKE) PRESSURE AFTER SUBSEA START-UP (psi) =  $\text{Shut In Casing Pressure}_{\text{psi}} - \text{Choke Line Friction Loss}_{\text{psi}}$
32. BOYLES LAW FORMULAE  $P_1 \times V_1 = P_2 \times V_2$   $P_2 = \frac{P_1 \times V_1}{V_2}$   $V_2 = \frac{P_1 \times V_1}{P_2}$  *Atmospheric Pressure. = 14.7<sub>psi</sub>*  
*P = Pressure: V = Volume*
33. BARRELS TO MCF CONVERSION =  $3 \text{ bpm} \times 8,086 \text{ cu ft/bbl*day} = 24,258 \text{ cu ft/day of gas}$

34. GAS MIGRATION RATE (*ft/hr*) = Shut-In Pressure Increase<sub>psi/hr</sub> ÷ Mud Gradient<sub>psi/ft</sub> *(can use SIDPP or SICP)*  
*(Increase over last hour)*
35. VOLUME TO BLEED DUE TO GAS MIGRATION (*bbls*) = (Working Pressure to Bleed<sub>psi</sub> ÷ Mud Gradient<sub>psi/ft</sub>) x Annular Capacity<sub>bbls/ft</sub>  
*(For Volumetric Method)*
36. LENGTH OF WET PIPE PULLED BEFORE FILL-UP FOR DESIRED PRESSURE DROP ΔP (*Length<sub>ft</sub>*)  
= (ΔP<sub>psi</sub> x Annulus Cap<sub>bbl/ft</sub>) ÷ [0.052 x MW<sub>ppg</sub> x (DP Cap<sub>bbl/ft</sub> + DP Displ<sub>bbl/ft</sub>)]
37. LENGTH OF DRY PIPE PULLED BEFORE FILL-UP FOR DESIRED PRESSURE DROP ΔP (*Length<sub>ft</sub>*)  
= [ΔP<sub>psi</sub> x (Annulus Cap<sub>bbl/ft</sub> + DP Cap<sub>bbl/ft</sub>)] ÷ 0.052 x MW<sub>ppg</sub> x DP Displ<sub>bbl/ft</sub>
38. HYDROSTATIC PRESSURE DROP PER FOOT (ΔP<sub>psi/ft</sub>) WHEN PULLING WET PIPE  
= 0.052 x MW<sub>ppg</sub> x [(DP Cap<sub>bbl/ft</sub> + DP Displ<sub>bbl/ft</sub>) ÷ Annulus Cap<sub>bbl/ft</sub>]
39. USABLE FLUID VOLUME PER BOTTLE  
= [(Precharge Pressure ÷ Minimum Operating Press) - (Precharge Pressure ÷ Maximum Operating pressure)] x Bottle Volume
40. BOP CLOSING RATIO (RAM BOP) = Piston Area ÷ Ram Shaft Area
41. CONVERSION OF API GRAVITY (°API) TO SPECIFIC GRAVITY (SG) = 141.5 ÷ (°API + 131.5)
42. CONVERSION OF SPECIFIC GRAVITY (SG) TO PPG = 8.33 x SG

## WELL COMPLETION/WORKOVER FORMULA SHEET—FIELD UNITS

1. KILL FLUID WEIGHT (*ppg*) =  $[SITP_{psi} \div 0.052 \div \text{Top Perfs TVD}_{ft}] + \text{Original Fluid Weight}_{ppg}$
2. KILL FLUID WEIGHT (*ppg*) =  $BHP_{psi} \div 0.052 \div TVD_{ft}$
3. BUOYANCY FACTOR (*BF*) =  $(65.4 - \text{Fluid weight}_{ppg}) \div 65.4$
4. PIPE WEIGHT BUOYED—OPEN ENDED PIPE (*lbs/ft*)  
=  $\text{Weight}_{air, (lbs/ft)} \times \text{Buoyancy Factor}$
5. BUOYED WEIGHT OF TUBULARS (CLOSED ENDED & NO FLUID IN PIPE) (*lbs/ft*)  
=  $\text{Weight}_{air, (lbs/ft)} - [(\text{Pipe OD}_{in}^2 \times \text{Fluid weight}_{ppg}) \div 24.5]$
6. BUOYED WEIGHT OF TUBULARS (DIFFERENT FLUID IN PIPE AND ANNULUS) (*lbs/ft*)  
=  $\text{Weight}_{air, (lbs/ft)} + [(\text{Pipe ID}_{in}^2 \times \text{Fluid weight}_{tbg}) \div 24.5] - [(\text{Pipe OD}_{in}^2 \times \text{Fluid weight}_{Annulus}) \div 24.5]$

### BULLHEADING FORMULAE

7. FORMATION FRACTURE PRESSURE (*psi*) =  $\text{Formation Fracture Gradient}_{psi/ft} \times \text{Top Perforations TVD}_{ft}$
8. INITIAL HYDROSTATIC PRESSURE (*psi*) =  $\text{Formation Pressure}_{psi} - SITP_{psi}$
9. INITIAL AVERAGE FLUID DENSITY (*ppg*) =  $\text{Initial Hydrostatic Pressure}_{psi} \div \text{Top Perforations TVD}_{ft} \div 0.052$
10. MAX INITIAL SURFACE PRESSURE (*psi*) =  $\text{Formation Fracture Pressure}_{psi} - \text{Initial Hydrostatic Pressure}_{psi}$
11. MAX FINAL SURFACE PRESSURE (*psi*) =  $\text{Formation Fracture Pressure}_{psi} - (\text{Kill Fluid Weight}_{ppg} \times 0.052 \times \text{Top Perforations TVD}_{ft})$
12. VOLUME TO BULLHEAD (*bbls*) =  $\text{Surface Lines}_{bbls} + \text{Surface to EOT}_{bbls} + \text{EOT to Top Perfs}_{bbls} + \text{Top Perfs to Bottom Perfs}_{bbls}$   
*{EOT = End of Tubing                      Perfs = Perforations}*
13. BULLHEAD SPM TO EXCEED GAS MIGRATION =  $(\text{Gas Migration Rate}_{ft/hr} \div 60) \times \text{Tubing Capacity}_{bbls/ft} \div \text{Pump Output}_{bbls/stroke}$

**TEMPERATURE CORRECTION FORMULA FOR BRINES**

14. AVERAGE TEMPERATURE

$$= (\text{Bottomhole Temp}_F + \text{Surface(Ambient) Temp}_F) \div 2$$

*{Avg = Average}*

*F = degrees Fahrenheit}*

15. FLUID DENSITY TO MIX (ppg)

$$= \text{Fluid Density at Avg. Temp}_{\text{ppg}} + [(\text{Avg. Temp}_F - \text{Surface Temp}_F) \times \text{Weight Loss}_{\text{ppg}/^\circ\text{F}}]$$

*{Avg = Average}*

*F = degrees Fahrenheit}*

**Example Weight Loss Chart**  
 (Note: Values will vary based on type of fluid and other factors.)

Brine weight (ppg)	Weight loss (ppg/°F)
8.4 – 9.0	0.0017
9.1 – 11.0	0.0025
11.1 – 14.5	0.0033
14.6 – 17.0	0.0040
17.1 – 19.2	0.0048